

Research Paper

High Production of 2,3-butanediol by a Mutant Strain of the Newly Isolated *Klebsiella pneumoniae* SRP2 with Increased Tolerance Towards Glycerol

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Abstract

Biodiesel, a renewable fuel produced by transesterification of animal fats and vegetable oils, generates about 10% (v/v) of crude glycerol as a core byproduct. The high volume of this non bio-degradable glycerol is becoming of a great environmental and economical concern due to its worldwide ever-growing surplus. Herein we report a high production of 2,3-butanediol (2,3-BD) from pure and biodiesel derived crude glycerol using a mutant *K. pneumoniae* SRM2 obtained from a newly isolated strain *Klebsiella pneumoniae* SRP2. The mutant strain SRM2 with standing high glycerol concentration (220 g L⁻¹ of medium) could rapidly convert glycerol aerobically to 2,3-BD, a versatile product extensively used in chemical, pharmaceutical and fuel industries. Our study revealed that an increased GDH activity led to a substantially enhanced production of 2,3-BD. The mutant strain exhibited 1.3-fold higher activity of GDH than that of parent strain (500.08 vs. 638.6 μmol min⁻¹ mg⁻¹ protein), yielding of 32.3 g L⁻¹ and 77.5 g L⁻¹ 2,3-BD with glycerol in batch and fed-batch process respectively. However, in batch culture with crude glycerol, cell growth and glycerol consumption were expressively boosted, and 2,3-BD production was 27.7 g L⁻¹ from 75.0 g/L crude glycerol. In this report, the optimal conditions for high production of 2,3-BD were defined in a completely aerobic process, and 0.59 g g⁻¹ product yield of 2,3-BD was attained by the mutated strain *K. pneumoniae* SRM2, which is the highest amount obtained from batch biotransformation process of glycerol metabolism till today. These results indicated that our newly developed mutant can tolerate high concentration of glycerol, have a high glycerol utilization rate, and high product yield of 2,3-BD. It is demonstrated that the mutant strain *K. pneumoniae* SRM2 has an ability to produce fewer co-products at trace concentrations at higher glycerol concentrations, and could be a potential candidate for 2,3-BD production in an industrial bioconversion process.

Key words: Glycerol dehydrogenase, Crude glycerol, 2,3-Butanediol, Bioconversion, *Klebsiella pneumoniae*.

Introduction

Biodiesel has become one of the vibrant renewable fuels produced from animal fats and vegetable oils by reacting with a primary alcohol in the presence of an alkali or acid catalyst. During the last few years, biodiesel production has increased dramatically, and a significant amount (10% v/v) of crude glycerol is generating from a typical biodiesel

production process. Crude glycerol produced from bio-refineries is a worldwide overflow problem due to a nonexistence of refining capacity. Thus, a high volume of crude glycerol is the key problem for growth of biodiesel industry. The economic feasibility of the biodiesel industry has been crucially affected due to a high volume (by worldwide surplus) of crude

glycerol generated from biodiesel production process [1]. Therefore, with increasing biodiesel production plants, a large number of glycerol production plants will be shut down within few years due to price drop by oversupply of glycerol [2, 3] that require new commercial uses. Glycerol, a core by-product of biodiesel production has become an inexpensive and easily obtainable product for which new applications have to be discovered [1]. Several species of Enterobacteriaceae are capable for converting glycerol to produce value-added bio-products [5-7]. Until now, there is no effectual microorganism which can convert glycerol efficiently to produce industrially important high-priced products. Most of the studies have been carried out on bioconversion of glycerol using anaerobic fermentation process [1, 7]. Our primary focus is to enhance the production of 2,3-BD from glycerol by effective bacterial strain under completely aerobic process. However, for glycerol metabolism, the metabolic pathways of *K. pneumoniae* has been explored recently [8]. In *K. pneumoniae*, the metabolic process of glycerol bioconversion is accomplished by a complex two-branch (oxidative and reductive)

pathways (Fig. 1), which results in the synthesis of major products including dihydroxyacetone (DHA), 2,3-BD, ethanol, acetoin, acetate and 1,3-propanediol (1,3-PDO). In the oxidative branch, an important cell-bounded (intracellular) and NAD⁺-dependent enzyme GDH converts glycerol to DHA, producing NADH as a reducing equivalent [4, 8]. Subsequently, dihydroxyacetone phosphate (DHAP) is generated from DHA by ATP or phosphoenolpyruvate-dependent DHA kinase, which is then further metabolized to various products through pyruvate [4, 8]. Meanwhile, NADH (reducing equivalent) produced after receiving electrons from oxidation of substrate organic compounds could stimulate 1,3-PDO production [8]. Moreover, glycerol is firstly converted to 3-hydroxypropionaldehyde (3-HPA) by the coenzyme B₁₂-dependent glycerol dehydratase through the parallel reductive branch of glycerol metabolism, and it is then reduced to the major product 1,3-PDO by the NADH-linked 1,3-PDO dehydrogenase, thereby regenerating NAD⁺ [4, 8].

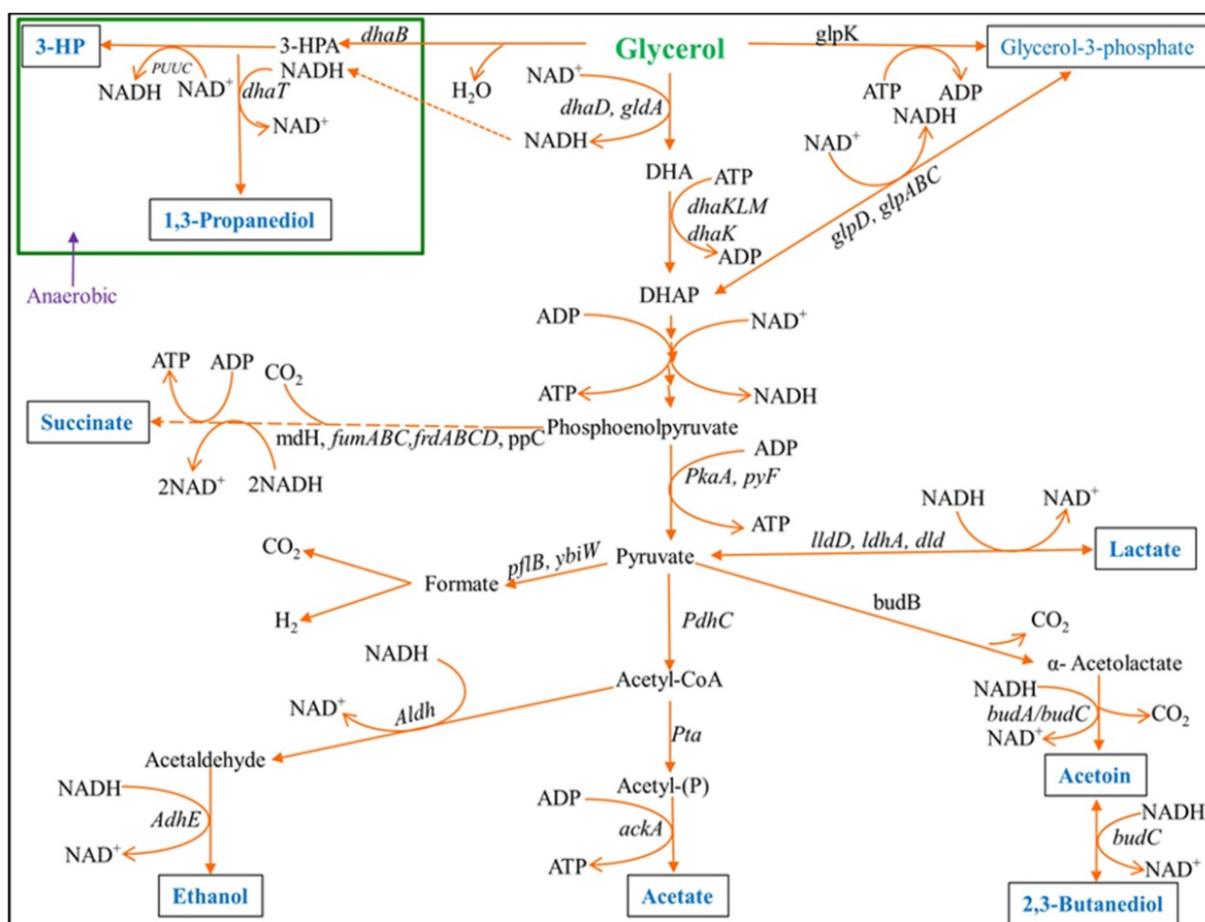


Figure 1. Initial steps of the glycerol dissimilation pathway together with 2,3-BD, 1,3-PDO, acetate and acetoin formation in *Klebsiella*. 3-HP: 3-Hydroxypropionic acid.

The two important platform chemicals 2,3-BD and acetoin can be obtained from oxidative pathways of glycerol metabolisms of many bacteria [6, 9]. Acetoin, an important metabolic product of microorganisms is commonly used for the preparation of cosmetics, food, and many chemicals [10]. However, 2,3-BD is an expensive chemical which is used as a liquid fuel and fuel additive [11]. As an industrially important chemical, 2,3-BD is also extensively used for the preparation of pharmaceuticals and many synthetic materials [11, 12].

Recently, many species (*Klebsiella planticola*, *K. oxytoca* and *K. pneumoniae*) of the genus *Klebsiella* have been reported to produce 1,3-PDO as a principal product through bioconversion of glycerol, whereas 2,3-BD was the minor [9, 13-15]. In this study, metabolic products of batch and fed-batch fermentation of glycerol using a newly isolated strain *K. pneumoniae* SRP2 and its ethyl methane sulfonate (EMS) mutant was evaluated. Our goal was to optimize the culture conditions to gain expression of GDH as well as increase metabolic product yield of 2,3-BD to make a process relevant for industrial application. Here, we report a high product concentration of 2,3-BD from glycerol as a sole carbon source using our newly isolated strain *K. pneumoniae* SRP2 and its EMS mutant *K. pneumoniae* SRM2.

Materials and Methods

Isolation of glycerol degrading bacterial strain

K. pneumoniae SRP2 wild type and an EMS mutant SRM2 strains were used throughout this study. The strain *K. pneumoniae* SRP2 was isolated from paper mill waste of Resolute Forest Products, Canada. In order to isolate the glycerol degrading bacterial strain SRP2, the method described our earlier work [6] was followed. This isolated strain was further screened for their glycerol assimilation, GDH activity and 2,3-BD production. This strain was maintained at 4°C on Luria-Bertani (LB) agar slant and sub-cultured every two weeks.

Identification of the bacterial strain

The strain SRP2 was identified by 16S rDNA sequencing, confirmed by its phenotypic and biochemical characteristics. The gene encoding 16S rRNA was amplified from the genomic DNA of SRP2 strain by PCR (polymerase chain reaction) using 16S rDNA universal bacterial primer pairs, which were HDA-1 (5'-GACTCCTACGGGAGGCAGCAGT) and E1115R (5'-AGGGTTGCGCTCGTTGCGGG), and a 726 bp fragment was obtained. The product obtained after PCR was purified using PCR purification Kit (Geneaid, Canada) following the manufacturer's

protocol. The purified PCR sample was sent to Euroffins Genomics (USA) for sequencing. For identification of the strain SRP2, sequence analysis was performed using NCBI blast tool, compared with sequences of the Gene Bank database search (<http://www.ncbi.nlm.nih.gov/genbank/>). The phylogenetic relationship was analyzed using sequence alignment program ClustalX and TreeView software. The species identification was confirmed using phenotypic and biochemical features [16].

Optimization of fermentation parameters

Seed culture for batch and fed-batch processes was prepared from stock slant culture by inoculating into LB broth medium. The LB broth seed culture was incubated at 37°C and 180 rpm for 20 h. Following incubation, the seed culture was inoculated into appropriate medium for optimization of culture conditions such as incubation temperature and time, medium initial pH, glycerol concentration, and nitrogen sources. All the growth parameters were performed in triplicates. For GDH enzyme and 2,3-BD assay, batch fermentations were maintained in 250 ml Erlenmeyer flasks (100 ml medium and 100 µl of 20 h culture as the inoculum) at different initial pH (4, 5, 6, 7, 8 and 9), temperatures (25- 40°C), and at different concentrations of glycerol (25 - 65 g L⁻¹), yeast extract (1.0 - 5.0 g L⁻¹) and peptone (4.0 - 6.5 g L⁻¹). The minimal salt-1 (MS-1) medium (KCl, 0.1 g L⁻¹; K₂HPO₄, 0.1 g L⁻¹; MgSO₄ .7H₂O, 0.05 g L⁻¹ and NaNO₃, 0.1 g L⁻¹) supplemented with specified concentration of glycerol or crude glycerol and nitrogen sources was used throughout the experiments when indicated. Medium pH was adjusted using HCl(1 M)/NaOH (1 M). Biodiesel byproduct (crude glycerol) supplied by CARES (Centre for Agricultural Renewable Energy and sustainability) biodiesel plant (Guelph, Canada) was used as a feedstock (sole carbon source) for microbial growth throughout this study. This crude glycerol contains 50.0±4.6% glycerol.

Batch and fed-batch fermentation under optimized conditions

Batch and Fed-batch fermentations were carried out in 250 ml Erlenmeyer flasks containing 100 ml medium (initial pH 8.0) with 100 µl of 20h culture as the inoculum, incubated at 37°C under aerobic condition at 180-200 rpm. The medium MS-2 used for batch and fed-batch cultures contained KCl (0.1 g L⁻¹), K₂HPO₄ (0.1 g L⁻¹), MgSO₄ .7H₂O (0.05 g L⁻¹), NaNO₃ (0.1 g L⁻¹), glycerol (55.0 g L⁻¹) or crude glycerol (75.0 g L⁻¹), yeast extract (2.5 g L⁻¹) and peptone (4.5 g L⁻¹). In case of fed-batch culture, the glycerol concentrations were varied. In our fed-batch culture,

an initial concentration of glycerol was 55 g L⁻¹, and then a concentrated solution containing 800 g L⁻¹ of pure glycerol or crude glycerol was fed into the culture as required.

Enzyme Assay

The enzyme assay of membrane-bounded GDH was carried out by measuring the initial reduction rate of NAD (from NAD to NADH) at 340 nm absorbance according to the established method [17] with minor modifications [6]. The reaction mixture used for GDH assay contained ammonium sulfate (30 mM), glycerol (0.2 M), potassium phosphate buffer (50 mM) and NAD (1.2 mM), which was prepared just before the enzyme assay. A 96 well microplate (flat bottom), each well with 1 cm light path length containing 250 µl reaction mixture was used for GDH assay. The reaction was started by adding 50 µl cell free extract of bacterial cells. One unit of GDH activity is defined as the amount of enzyme required to oxidize 1 µmole of substrate per minute. However, the specific activity of GDH is stated as µmoles of substrate reduced/minute/mg of cell protein. Protein was quantified using standard protocol [18] with bovine serum albumin as a standard protein.

Strain development

An adapted strain was developed from the wild type strain SRP2 using the method described in our previous study [6]. This evolutionary developed (adapted) strain was able to grow at a concentration of 220 g L⁻¹ glycerol. The evolutionary adapted strain was mutagenized with UV coupled with EMS [19]. To get UV mutant, the inoculated culture plate was exposed to UV light at 280 nm wavelength for 3 minutes and 40 cm away from the light source. For EMS mutagenesis, the UV treated culture was used, and a standard method described by Jensen et al [20] was followed. Briefly, 0.1ml of 24h LB broth culture was plated on MS-1 agar medium supplemented with 100 g L⁻¹ glycerol. On the centre of the plate, a drop 6 µl EMS (99%) was placed, incubated at 37°C for 72h. Following incubation, a bacterial colony grown at the edge and middle of EMS inhibition zone was taken, streaked on MS-1 agar medium containing 100 g L⁻¹ glycerol, and tested its 2,3-BD product concentration.

Toxicity test

For toxicity test, the minimum inhibition concentration (MIC) and minimum bactericidal concentration (MBC) of glycerol were performed in batch culture. A series of culture medium (MS-1 supplemented with yeast extract 2.5 g L⁻¹) tubes were prepared with different concentrations of glycerol ranging from 100 to 550 g L⁻¹, inoculated with 100 µL of a 20 h culture, and incubated at 37°C for 120h.

Following incubation, growth was evaluated spectrophotometrically based on the absorbance at 600 nm and the dry cell mass was measured by using a standard curve (a linear correlation between the dry cell mass and absorbance of cell suspension). For MBC, 100 µL culture broth from each tube was plated on LB agar medium, and incubated at 37°C for 48h. After incubation, any growth was observed on the agar plate. All tests were conducted in at least triplicates.

Assay of biomass and metabolic products

Biomass was measured as absorbance at 600 nm using microplate spectrophotometer (EPOCH, BioTek) and converted to cell dry weight using a calibration equation ($y = 2.0978x - 0.0346$, where $y = OD_{600}$, $x = \text{biomass g L}^{-1}$) obtained from standard curve of a linear correlation between the dry cell mass and absorbance of cell suspension (Figure S1). The identity of the end products was confirmed by GC-MS (Varian 1200 Quadrupole). Glycerol concentration (g L⁻¹) and major metabolic products including 2,3-BD, acetoin, 1,3-PDO and acetic acid were determined by GC-FID (Shimadzu GC 14A) under the following conditions: sample volume 1 µl; column temperature range from 45°C (2 min) to 240°C at the rate of 10°C/min; the injector and detector temperature 250°C; carrier gas nitrogen; column DB-WAXetr. The injecting sample was purified by centrifugation and membrane filter (0.22 µm pores size).

Results

Isolation and identification of bacterial strain

The isolation procedure was primarily based on tolerance and ability to utilize glycerol (100 g L⁻¹) as the sole carbon source to produce GDH enzyme under aerobic condition, and yielded a number of bacterial strains from soil and paper mill waste samples. Of these isolates, the strain SRP2 (*K. pneumoniae*) isolated from paper mill waste exhibited significant GDH activity. This highly active SRP2 strain was identified as genus *Klebsiella* (99% similarity) using 16S rRNA gene sequencing. By using phenotypic and biochemical characters shown in Table 1, the species *K. pneumoniae* (strain *K. pneumoniae* SRP2) was identified. On LB agar the strain SRP2 was found to grow as large mucoid and slimy (old culture) colonies. The morphological features observed by light microscopy are: rod-shaped and encapsulated cells, 0.4 - 0.8 µm in diameter and 0.7-5.0 µm in length, arranged singly/ in pair/ in short chain.

The 16S rRNA sequences of the isolated strain SRP2 and its EMS mutant SRM2 have been submitted to the GenBank for accession numbers. The strains

reported in this research article have been nominated as *Klebsiella pneumoniae* SRP2 (wild) and *K. pneumoniae* SRM2 (mutant), and their GenBank accession numbers are released as KR092086 and KX572902 respectively. However, for the phylogenetic relationship analysis, the 16S rRNA gene sequences of SRP2 and its mutant SRM2 were aligned using ClustalX UPGMA algorithm and uploaded into TreeView (Fig. 2). The phylogenetic tree was built by the Neighbor-Joining method using 16S rRNA gene sequencing. The result of phylogenetic relationship confirmed that the strains belong to the genus *Klebsiella* or species *K. pneumoniae*. In phylogenetic tree the distance between the wild type (*K. pneumoniae* SRP2) and its mutant (*K. pneumoniae* SRM2) strains also confirmed mutagenesis.

Table 1. Morphological and physiological characters of strain *K. pneumoniae* SRP2

Characters	Results
Gram staining (24h)	Gram -
Capsule	+
Indole production	-
H ₂ S production	-
Methyl red	+
Voges-Proskauer	+
Citrate	+
Urea hydrolysis	+
Gas/acid from Lactose (44°C)	+/+
Gas/acid from glucose	+/+
Gelatin hydrolysis (22°C)	-
KCN growth	+
Nitrate reduction	+
Lysine decarboxilate	+
Oxidase	-
Catalase	+
Acid from cellobiose, maltose, mannitol, arabinose, sucrose and sorbitol.	+

+, positive; -, negative

Strain development

The adapted strain obtained from 220 g L⁻¹ glycerol was used to develop EMS mutant. Following

incubation, a zone of inhibition was developed on the plates around the drop of EMS (Fig. 3). All the colonies obtained from the edge and middle of the inhibition zone were streaked on MS-1 agar plates with 100 g L⁻¹ glycerol, and tested for their 2,3-BD production. The EMS mutagenesis revealed a high yielding 2,3-BD mutant marked as strain No. SRM2.

Effect of growth factors on GDH activity and 2,3-BD production in batch culture

In the oxidative pathway, GDH is a key enzyme for converting glycerol to biofuels and value-added metabolic products including DHA, 2,3-BD, acetoin and organic acids. To optimize glycerol concentration, incubation temperature and time, initial pH and nitrogen sources for maximum enzyme activity, experiments were carried out in batch fermentation (Fig 4-7). In this aerobic batch fermentation, glycerol was only the carbon source for microbial growth to produce GDH and 2,3-BD. The results revealed optimum initial concentrations 45 g L⁻¹ and 55 g L⁻¹ of glycerol for the strains SRP2 and SRM2 respectively, whereas the yeast extract concentration was 2.5 g L⁻¹ at starting pH 7.0 and incubation temperature 37°C (Fig 4). To optimize the incubation temperature for maximum GDH activity and 2,3-BD production of the both strains SRP2 and SRM2, experiments were performed in batch culture at starting pH 7.0 under controlled temperatures ranging from 25 to 40°C. The maximum enzyme activities 344.5 and 467.7 unit/mg protein were achieved at 37°C after 48h incubation with the strains SRP2 and SRM2 respectively (Fig. 5). In case of 2,3-BD, the maximum concentrations 12.9 g L⁻¹ and 15.0 g L⁻¹ of 2,3-BD were attained by the strains SRP2 and SRM2 respectively at the same temperature under the same conditions (Fig. 5). The mutant strain SRM2 exhibited 1.35 and 1.16-fold higher production of GDH and 2,3-BD respectively compared to that of its wild type SRP2 strain under same incubation conditions.

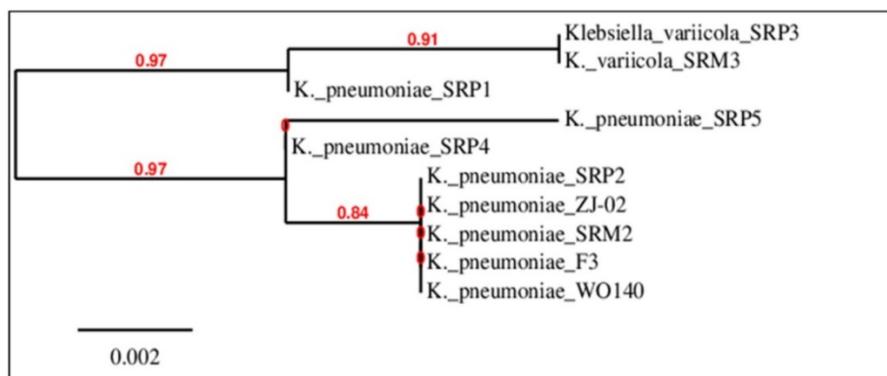


Figure 2. Phylogenetic tree drawn from ClustalX alignment, presented in TreeView.

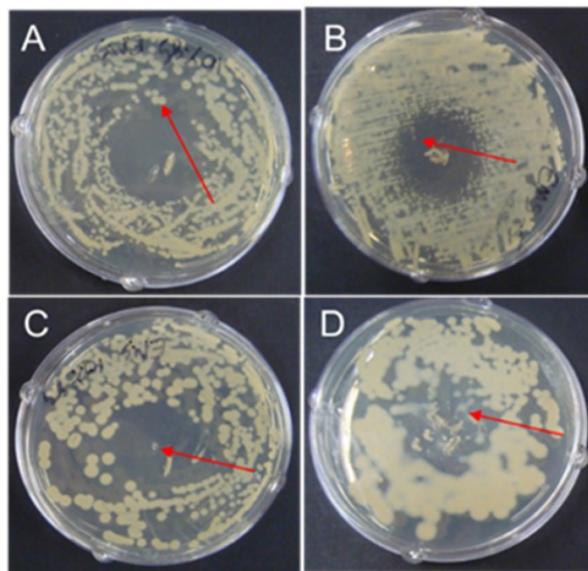


Figure 3. EMS treated culture plates A, B, C and D for possible mutant.

The initial pH of the medium played an important role for the production of GDH and 2,3-BD by SRP2 and SRM2 strains. Experiments without pH control showed that the higher was the starting pH values, the greater was the GDH activity and 2,3-BD concentration (Fig. 6a). Before autoclaving, the medium pH values (4-8) were adjusted using HCl/NaOH. A time course of pH and cell biomass changes with starting pH 8.0 was performed over a period of 144 h (Fig. 6b). Fascinatingly, in the first 24 h, the pH of the medium speedily dropped and reached values from 8.0 to 4.6. This first 24 h incubation period was the exponential growth phase

of the batch culture and the pH was dropped due to the production of acetate and/ other organic acids in the culture medium. After 24 h incubation, the pH values were slightly rose and dropped during incubation and reached values between 4.6 and 5.5 due to production of 2,3-BD. Figure 6a shows that the maximum GDH activity (522.5 unit/mg protein) and 2,3-BD (17.5 g L⁻¹) production were attained at initial pH 8.0 by SRM2.

In addition to yeast extract (2.5 g L⁻¹), experiments were carried out on the effect of other nitrogen sources viz., malt, peptone, NH₄NO₃, (NH₄)₂SO₄ and NH₄Cl for GDH and 2,3-BD production with the wild type strain SRP2 and its mutant SRM2. The peptone showed the highest GDH activity (616.7 unit/mg protein) and 2,3-BD product concentration (19.21 g L⁻¹) compared to that of other nitrogen sources with SRM2 strain (Fig 7a). The maximum GDH activity 638.6 unit/mg protein and 22.8 g L⁻¹ were attained at a concentration of 4.5 g L⁻¹ peptone after 48 h incubation by SRM2 (Fig. 7b).

Toxicity test

The mutated strain SRM2 was used for a toxicity test towards different concentrations of glycerol (Fig. 8). At an initial glycerol concentration of 300 g L⁻¹, growth of SRM2 was detectable after 120 h incubation. However, at an initial glycerol concentration of 450 g L⁻¹, viability of SRM2 strain was also detectable after cultured on LB agar. Based on these results strain SRM2 seemed most tolerant to glycerol. MIC and MBC of glycerol were determined as 350 g L⁻¹ and 500 g L⁻¹ respectively (Fig. 8).

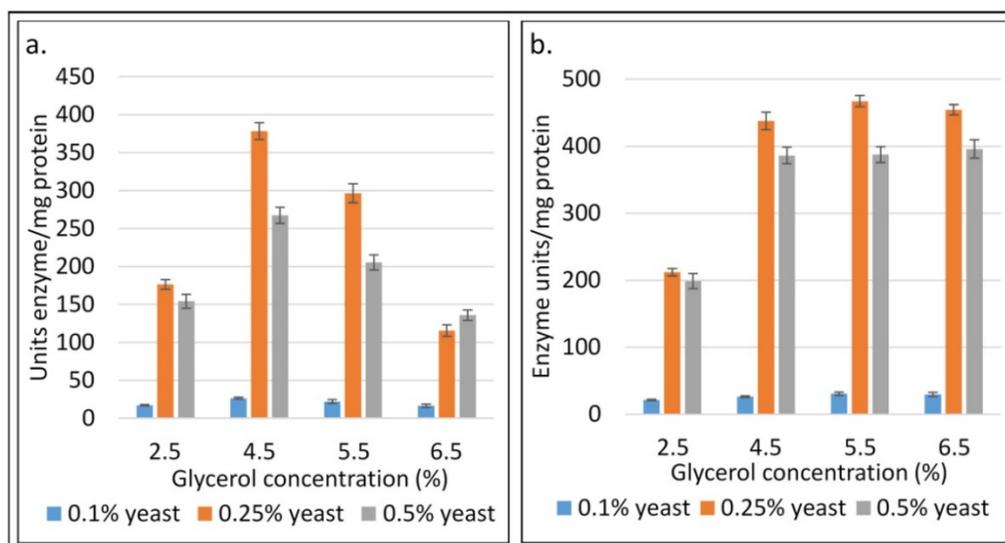


Figure 4. Influence of the concentrations of glycerol and yeast extract on GDH activity after 48h at 37°C and initial pH 7.0. (a) Wild type *K. pneumoniae* SRP2 (b) Mutant SRM2.

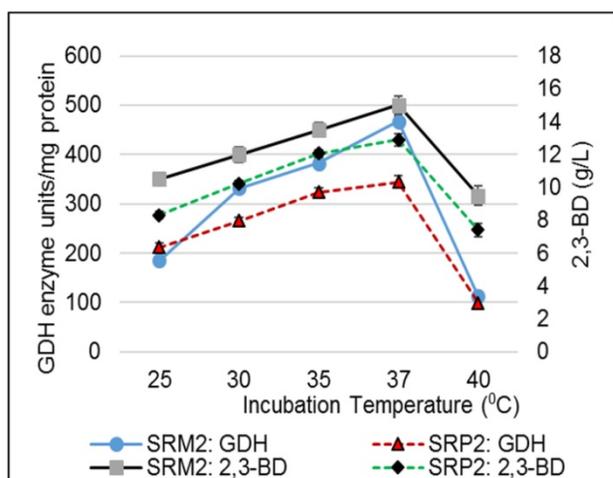


Figure 5. Influence of temperature on GDH activity and production of 2,3-BD of *K. pneumoniae* SRP2 and its mutant SRM2 after 48h at 37°C. MS-1 medium with glycerol 55.0 g L⁻¹ and yeast extract 2.5 g L⁻¹ was used. Medium initial pH was 7.0.

Batch and fed-batch process under optimized conditions

Batch and fed-batch cultivation processes were carried out under optimized conditions for maximizing 2,3-BD production. To investigate glycerol utilization and 2,3-BD production by *K. pneumoniae* SRP2 and its EMS mutant *K. pneumoniae* SRM2, batch cultures were performed with pure glycerol or crude glycerol as the sole carbon source at the initial concentration of 55.0 g L⁻¹ and 75.0 g L⁻¹ respectively. For quantification of bio-products, experiments were set at initial pH 8.0 and temperature 37°C. The medium used for both batch and fed batch cultures was MS-2. The above culture conditions revealed two major products 2,3-BD and

acetoin with other minor products including 1,3-PDO and acetate. In our batch process, a typical outline for aerobic bioconversion of pure glycerol by SRP2 and its mutant SRM2 at different incubation time, and production of end products are summarized in the Fig. 9. The *K. pneumoniae* SRP2 in this paper, utilized 100% of glycerol after 144 h, generating 20.55±1.22 g L⁻¹ 2,3-BD, 4.34±0.87 g L⁻¹ 1,3-PDO and 8.52±0.76 g L⁻¹ acetoin in batch process. The maximum concentration and yield of 2,3-BD attained after 120 h incubation were 28.53±1.34 g L⁻¹ and 0.52 g/g glycerol respectively (Fig. 9a). Nevertheless, a maximum 32.3 g L⁻¹ of 2,3-BD was obtained from 55 g L⁻¹ glycerol after 120 h incubation by SRM2, and the product yield was 0.59 g g⁻¹ glycerol. The strain SRM2 utilized 100% of glycerol after 120 h incubation and the concentrations of major bio-products other than 2,3-BD determined in this batch culture after 120 h incubation were acetoin and 1,3-PDO, with concentrations, 6.7±0.64 g L⁻¹ and 3.22±0.25 g L⁻¹ respectively (Fig. 9b). SRM2 obtained from SRP2 by EMS mutagenesis was capable of grow in a high concentration (220 g L⁻¹) of glycerol. Thus, the better adapted mutant strain SRM2 could efficiently convert glycerol to 2,3-BD and acetoin compared to that of its wild type strain SRP2. The maximum product concentrations and glycerol consumption were achieved from 96h to 120 h incubation. In our batch culture, the highest concentrations of 1,3-PDO and acetoin obtained after 144 h were 3.56± 0.73 g L⁻¹ and 8.3±1.07 g L⁻¹ respectively for SRM2, and 4.34± 0.82 g L⁻¹ and 8.52±1.14 g L⁻¹ respectively for SRP2 (Fig. 9a and 9b). The major metabolic products obtained from this batch process of SRP2 and SRM2 were 2,3-BD, acetoin and 1,3-PDO, with a minor product acetic acid.

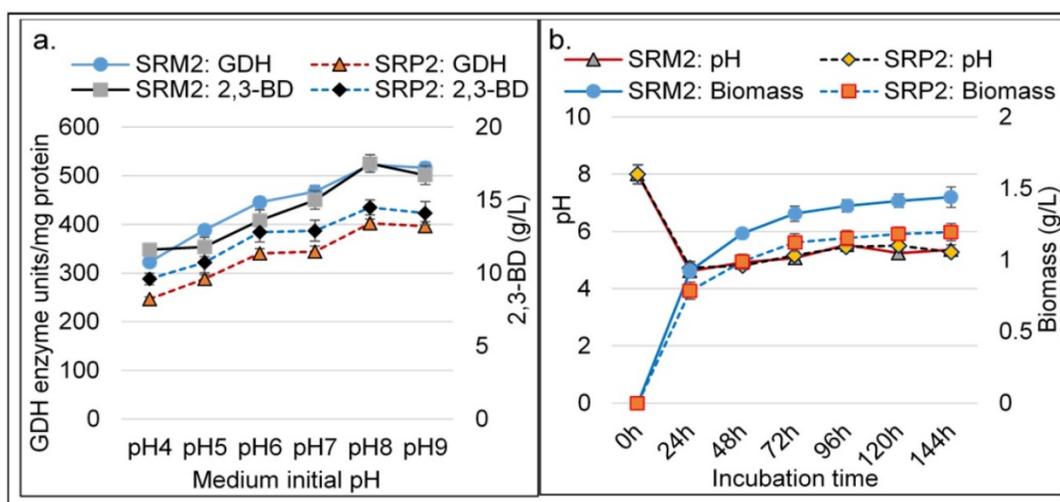


Figure 6. Effect of initial (starting) pH on *K. pneumoniae* SRP2 and its mutant SRM2 at 37°C. (a) GDH and 2,3-BD production after 48h incubation. (b) Time profile of pH fluctuation and biomass production. MS-1 medium with glycerol 55.0 g L⁻¹ and yeast extract 2.5 g L⁻¹ was used.

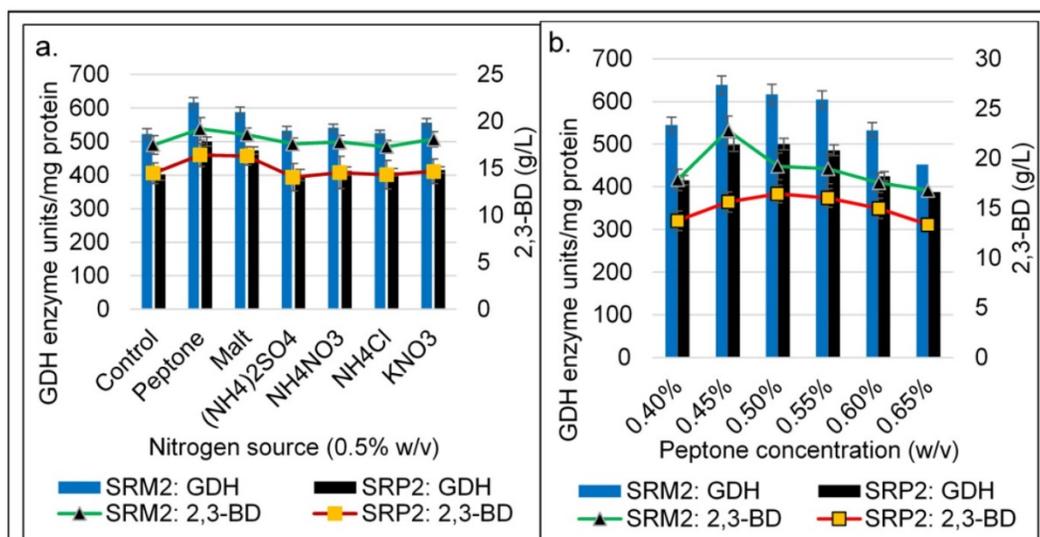


Figure 7. Influence of different nitrogen sources and peptone concentration on GDH and 2,3-BD production of *K. pneumoniae* SRP2 and its mutant SRM2 after 48h at 37°C. (a) Nitrogen sources. (b) Concentrations of peptone. MS-I medium with glycerol 55.0 g L⁻¹ and yeast extract 2.5 g L⁻¹ was used. Medium initial pH was 8.0.

To evaluate glycerol utilization and 2,3-BDO production from biodiesel derived crude glycerol (glycerol 50±4.6%, MONG 36.2±3.3, ash 4.2±0.3% and water 6.7±1.05%) by strains SRP2 and SRM2, batch process was carried out at initial concentrations of 50.0 -100.0 g L⁻¹ of crude glycerol (Figure S2). The optimal concentration of this crude glycerol was attained as 75.0 g L⁻¹ for maximum product concentration of 2,3-BD. The effect of incubation time on SRP2 and SRM2 strains for accumulation of major products in a batch culture process of crude glycerol are presented in the Fig. 10. As shown in Figure 10, the performance of the 2,3-BD production by SRM2 was higher than compared to that of wild type strain SRP2. Overall, the mutated strain SRM2 could produce 27.7±0.83 g L⁻¹ 2,3-BDO as the principal product using 38.25 g glycerol after 120h incubation

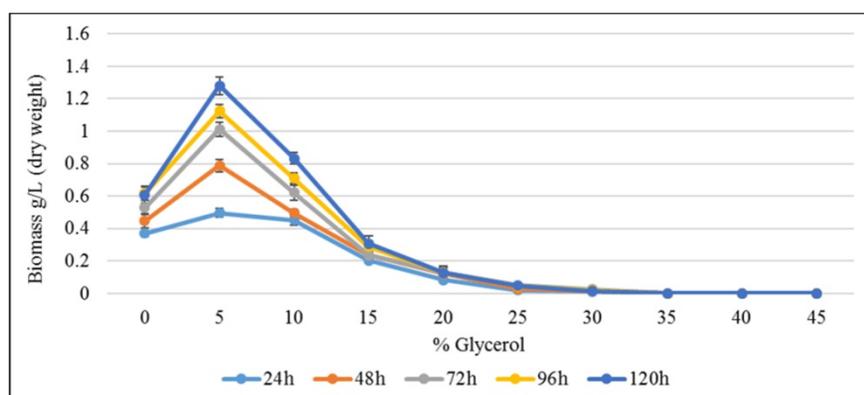


Figure 8. Toxicity [Minimum inhibitory concentration (MIC)] of glycerol against *K. pneumoniae* mutated strain SRM2 at initial pH 8.0. Incubation temperature was 37°C. MS-I medium with yeast extract 0.25% and peptone 0.45% was used.

(Fig. 10a). In this batch culture process, the highest concentrations of acetoin, 1,3-PDO and acetate obtained after 144 h were 5.78±0.21, 2.79±0.2 and 0.402±0.019 g L⁻¹ respectively with the strain SRM2 (Fig. 10b). However, the strain SRP2 exhibited the highest 2,3-BD production (25.73±1.04 g L⁻¹) after 120h incubation using 35.4 g glycerol (Fig. 10a).

In fed-batch process without pH control, the bioconversion kinetics showed that SRM2 produced high concentration of the principal product 2,3-BD in aerobic condition. Comparison between the final values of glycerol or biodiesel derived crude glycerol consumed, the biomass and major end products obtained by wild type strain SRP2 and EMS mutant SRM2 in fed-batch process are presented in Table 2. Table 2 shows that 51.1±1.7 g L⁻¹, a high production of 2,3-BD was obtained after 240 h incubation, consumed 77.4 g glycerol from 148.8 g L⁻¹ biodiesel derived crude glycerol by SRM2. In case of pure glycerol, the highest concentration of 2,3-BD (77.51±2.03 g L⁻¹) obtained after 240 h incubation by consumed 132.0 g glycerol. However, the wild type strain SRP2 exhibited 54.3±1.1 g/L 2,3-BD by consumed 91.1 g glycerol after 192h incubation.

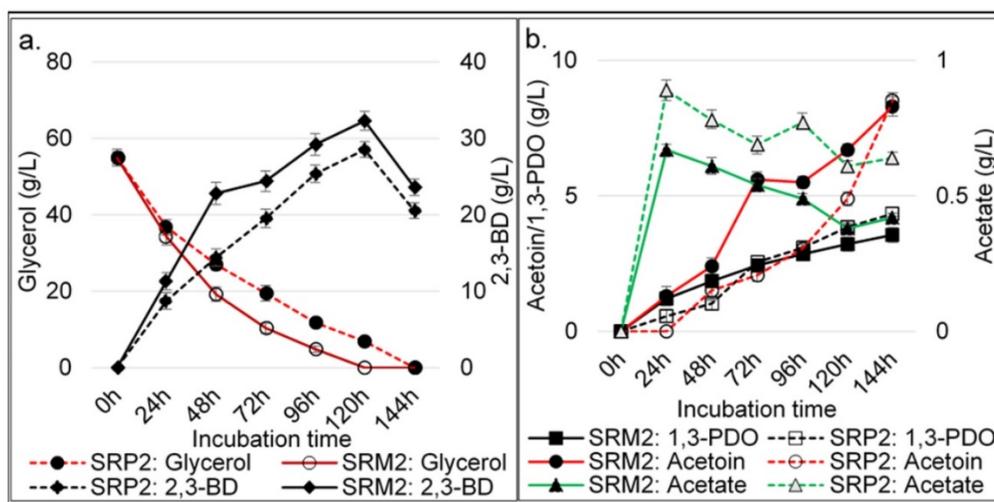


Figure 9. Time course data and metabolic products of batch cultivation at 37°C by wild type strain SRP2 and its mutant SRM2 of *K. pneumoniae*. (a) Glycerol and 2,3-BD concentrations. (b) Acetoin, 1,3-PDO and acetate concentrations. MS-2 medium with pure glycerol 55.0 g L⁻¹ was used. Medium initial pH was 8.0.

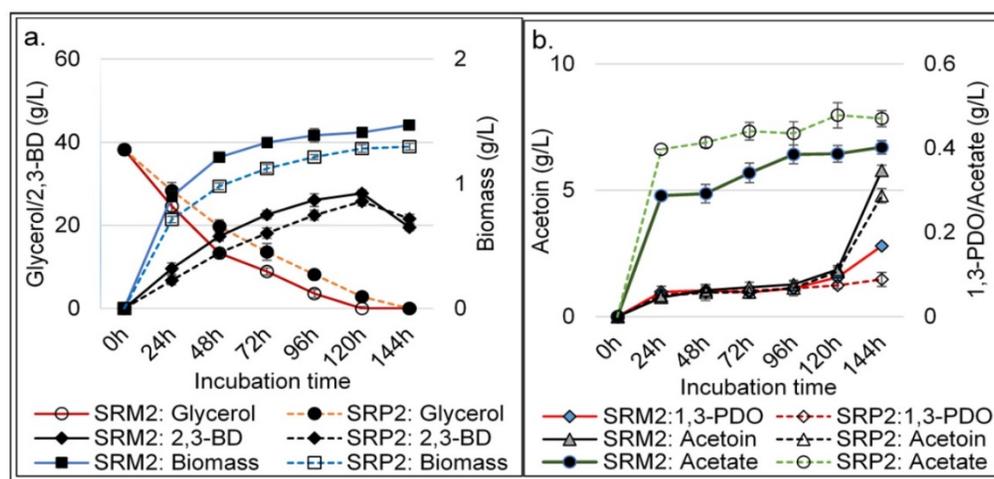


Figure 10. Time course data and metabolic products of batch cultivation at 37°C by wild type strain SRP2 and its mutant SRM2 of *K. pneumoniae*. (a) Glycerol and 2,3-BD concentrations. (b) Acetoin, 1,3-PDO and acetate concentrations. MS-2 medium with biodiesel derived crude glycerol 75.0 g L⁻¹ was used. Medium initial pH was 8.0.

Table 2. Comparison the final values of major products obtained from metabolized of glycerol by *K. pneumoniae* SRP2 and SRM2 strains in feed-batch process at initial pH 8.

Strain	Duration (Hour)	Final pH	Biom. (g/L)	Glycerol utilized (g/L)	2,3-BD		Acetoin		1,3-PDO	
					(g/L)	Yield (g/g)	(g/L)	Yield (g/g)	(g/L)	Yield (g/g)
SRP2	192	5.46	1.49	91.1	54.3±1.1	0.60	6.1±0.6	0.07	2.22±0.06	0.02
SRM2	240	5.74	1.68	132.0	77.5±2.0	0.59	7.8±0.5	0.06	1.76±0.05	0.01
°SRP2	192	6.52	1.63	68.82	40.2±1.7	0.58	4.4±0.2	0.06	1.23±0.04	0.02
°SRM2	240	6.12	2.17	77.4	51.1±1.7	0.66	5.5±0.4	0.07	1.85±0.12	0.02

All experimental values presented are mean values from triplicate experiments;

Biom.: Dry weight of biomass;

°Crude glycerol was used as carbon source for this strain

Discussion

With the thriving of biodiesel industry, global surplus of glycerol is increasing [1,21]. Due to oversupply of crude glycerol from biodiesel refinery the glycerol price would be significantly affected, and

several glycerol production plants will be shutdown [22]. Therefore, bioconversion of glycerol to value-added bio-products would lead to both environmental and economic dividends of biodiesel plant. Microbial conversion of glycerol to valuable chemicals is a subject of interest in the last few years

[23,24]. Considering the glycerol bioconversion into biofuels and value-added bio-products, most of the recent studies focused on anaerobic fermentation process, and many microorganisms are able to utilize glycerol as a sole carbon source anaerobically [20,24]. Recently, several attempts have been made to produce value-added metabolic products including ethanol, 1,3-PDO and H₂ from glycerol under anaerobic fermentation process [23,25], but very limited studies have been done for aerobic processes. There is no any external electron acceptor in anaerobic fermentation, and the microbial growth is hampered. To overcome this problem in an anaerobic process, this study may be a viewpoint for high production of 2,3-BD as a major product of glycerol conversion in an aerobic process, and turning 1,3-PDO into a minor by-product. Considering economic utilize of glycerol, a goal was achieved to isolate an effectual bacterial strain, and develop the strain for high yield of 2,3-BD from crude and pure glycerol conversion.

K. pneumoniae, an enteric bacterium has long been considered to produce 1,3-PDO from glycerol as a feedstock in an anaerobic process [7,15]. Recently, a few works have been done on 2,3-BD production in an aerobic process [12,26]. We have demonstrated, however, that our newly isolated strain *K. pneumoniae* SRP2, and its mutants SRM2 could aerobically metabolize glycerol in a GDH-dependent oxidative pathway, and produce significant amount of industrially important product 2,3-BD together with other minor co-products. Furthermore, keeping the conditions defined in this study, the high production 32.3 gL⁻¹ and 77.51 gL⁻¹ of 2,3-BD was achieved from batch and fed-batch processes respectively by the mutant SRM2, as these amounts were the highest obtained from glycerol conversion reported. Therefore, in this study, the batch process with 55.0 g L⁻¹ of initial glycerol was the optimal concentration for maximum GDH activity and 2,3-BD production, which is the highest glycerol concentration in batch culture (Fig. 5). Recently, Petrov and Petrova [26] studied on glycerol bioconversion by *K. pneumoniae* in fed-batch process, and showed the highest concentration 70.0 gL⁻¹ of 2,3-BD as well as 0.53 g/g product yield. Interestingly, the mutant strain grew on and tolerated a high glycerol concentration up until 220.0 gL⁻¹. Moreover, the glycerol, a feed stock for 2,3-BD production is less toxic to the mutant due to its high MIC and MBC values. This research confirmed that a high glycerol concentration, up until 55 g/L of feedstock concentration displayed maximum production yield of the metabolic product 2,3-BD, which could be the new prospect of glycerol bioconversion field.

Chemical mutagenesis, is a well-known and

extensively used method for increasing tolerance towards an inhibitor of a microbial strain. Therefore, this increased tolerance may lead down-regulation of gene(s) accountable for the expected product [27]. EMS, a widely used chemical mutagen induces base replacements or deletions of DNA in a bacterium [28, 29] that may then gain an ability of higher productivity of a targeted product [23, 31]. Our achievement with increased tolerance towards glycerol and increased 2,3-BD production by EMS mutagenesis confirmed the competence of EMS for development of *K. pneumoniae* SRM2 mutant.

In our batch process of *K. pneumoniae* SRM2, maintained at different initial pH levels (pH 4-9), discovered that slightly alkaline pH 8 was more favorable for the synthesis of 2,3-BD. This aerobic bioconversion of glycerol evidenced that the amount of the produced 2,3-BD from glycerol depends on the initial pH as well as other factors like temperature, initial concentration of glycerol and nitrogen sources.

We have demonstrated, however, that *K. pneumoniae* can utilize glycerol to produce 2,3-BD through oxidative pathway in a GDH-dependent manner. Clearly, the GDH enzyme plays a key role in oxidative pathway of glycerol metabolism and 2,3-BD formation. The establishment of optimal conditions including pH, incubation temperature and nitrogen sources for 2,3-BD synthesis must comprise enhancement of GDH in oxidative pathway of the bioconversion process of glycerol.

Conclusion

Under aerobic conditions, 2,3-BD production from glycerol by *K. pneumoniae* mutant resulted in increased product yield and concentration in culture medium. The mutant strain *K. pneumoniae* SRM2 can tolerate high concentration of glycerol, have a high glycerol utilization rate, and high product yield of 2,3-BD. It is demonstrated that *K. pneumoniae* SRM2 has an ability to produce fewer co-products at trace concentrations at higher glycerol concentrations. Thus, the mutated strain SRM2 is a better organism for the aerobic conversion of glycerol to 2,3-BD. Therefore, we can conclude that it can metabolize high concentrations of glycerol and effectively convert the same to 2,3-BD and acetoin.

Supplementary Material

Supplementary figures and tables.

<http://www.ijbs.com/v13p0308s1.pdf>

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Competing Interests

The authors have declared that no competing interest exists.

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